PRODUCTION OF HYDROGEN AND HYDROCARBON FROM CELLULOSE AND WATER

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 $\rm H_2$, $\rm CH_4$ and CO are produced by the thermal reaction (300°C) of cellulose and water vapor using Pt, $\rm Pt\text{-}TiO_2$ and $\rm Ru/SiO_2$ as catalysts, among which the $\rm Ru/SiO_2$ catalyst showed the highest activity for direct production of $\rm CH_4$ and $\rm H_2$.

The synthesis of hydrocarbons from CO and $\rm H_2$ or the direct methane formation from carbon and water has been one of the most important problems in catalysis from the view-point of energy conversion. The raw materials of this reaction, coal or oil, are produced by the long-term accumulation of plants or animals. Thus the direct conversion of cellulose, an annually renewable resource, into a gaseous fuel is very attractive. Here we report that hydrocarbons are directly synthesized from cellulose and water by thermal catalytic reactions using supported metal catalysts around $300^{\circ}\rm C$.

Three kinds of catalysts were prepared as follows: 1) Pt; Pt black (Engelhardt), 2) Pt-TiO $_2$ (Pt 15 wt%); Pt black and TiO $_2$ (Katayama Kagaku) were mixed and grounded in an agate motar. 3) Ru/SiO $_2$ (Ru 4.5 wt%); Aqueous solution of RuCl $_3$ was impregnated into SiO $_2$ (Nihon Aerosil), dried and reduced by 100 Torr of H $_2$ at 450°C for 1 hr. All the catalysts were used after reducing them by 100 Torr of H $_2$ at 200°C for 1 hr, followed by an evacuation at the same temperature for 1 hr, after they were mixed with cellulose. The amount of Pt black, Pt-TiO $_2$ and Ru/SiO $_2$ used were 0.022, 0.15 and 0.07 g, respectively, in order that the molar ratio of metals to the cellulose was made constant. Cellulose (Toyo filter paper, 45-15 mg) was cut into small peacies (ca. 0.5 mm square) and mixed with each catalyst, so that the

powders of catalyst were spread over the cellulose.

Cellulose and catalyst were placed in a closed glass circulation reactor (200 ml) in the presence of water vapor from U trap (liquid $\rm H_2O$). Gaseous products during the reaction were collected by a trap of -196 and -96°C, and analysed by a mass spectrometer (Hitachi RMS-4).

Table 1 $\label{eq:Amount} \mbox{Amount of gaseous products and the conversion of cellulose to gases}$ after 150 min. of reaction at 300°C.

		gaseous products (%)					%
		Н ₂	CH ₄	CO	co ₂	C ₂ ⁺	conver -sion
neutral	Cellulose* itself	none	none	55.6	44.4	none	
	Pt-black	23.1	3.0	41.6	32.3	none	1.7
	Pt-TiO ₂ **	13.0	3.9	41.6	41.6	none	19.2
	after 1200 min	22.0	3.1	46.3	28.6	nonė	23.0
	Ru/SiO ₂	36.2	4.3	19.9	39.5	none	20.5
	after 1200 min	36.5	16.1	3.6	43.8	none	26.5
+ KOH***	Pt-black	72.9	5.1	0.07	none	21.9	10.0
	Pt-TiO ₂	64.6	3.2	0.45	none	31.7	26.6
	Ru/SiO ₂	89.8	2.9	1.3	none	5.4	32.2

- * Water produced were trapped during the decomposition.
- ** The amount of conversion in 150 min changed from 9.0 to 19.2% according to the catalysts used.
- *** ${\rm CO}_2$ produced in this system was dissolved into KOH.

Table 1 shows the total amount (%) and the component (%) of the gaseous products formed from cellulose in 150 min at 300°C. Cellulose itself decomposed slowly to form CO, ${\rm CO_2}$ and ${\rm H_2O}$ with no ${\rm H_2}$ produced in the absence of catalyst. It was, however, demonstrated that ${\rm H_2}$, CO, CH₄ and CO₂ were the main products in the presence of water vapor and the catalyst (Pt or Ru). When Ru catalyst was employed, the amount of CH₄ gradually increased with time, whereas in the case of Pt, the ratio of produced CH₄ to CO remained unchanged. It may be interpreted that CO and H₂

produced from cellulose and water reacted to form $\mathrm{CH_4}$ on the Ru surface, since Ru is a well-known catalyst for the $\mathrm{CH_4}$ formation from $\mathrm{CO} + \mathrm{H_2}^{1)}$. Accordingly, $\mathrm{Ru/SiO_2}$ exhibited the highest activity for the production of $\mathrm{CH_4}$ and $\mathrm{H_2}$ among these catalyst. The catalyst, $\mathrm{Pt}\text{-TiO_2}$ or $\mathrm{Ru/SiO_2}$ was more active than Pt black as is estimated from the amount of cellulose reacted (Table 1). The gaseous products were not observed at all at reaction temperature below 200°C.

The role of $\rm H_2O$ in the reaction is essential for the $\rm H_2$ production. When $\rm H_2O$ was present, the amount of CO produced decreased whereas $\rm H_2$ and $\rm CO_2$ increased. In the case of $\rm Ru/SiO_2$, the amounts of $\rm H_2$, CO and $\rm CO_2$ produced in 300 min without $\rm H_2O$ were 8.2, 20.8 and 10.6 µmol, respectively, whereas they were 90.3, 7.9 and 23.0 µmol with $\rm H_2O$ vapor (Fig 1). It suggests seemingly that water gas shift reaction, $\rm H_2O$ + CO + $\rm H_2$ + CO₂, occurs in the presence of $\rm H_2O$ over the Ru or Pt catalyst.

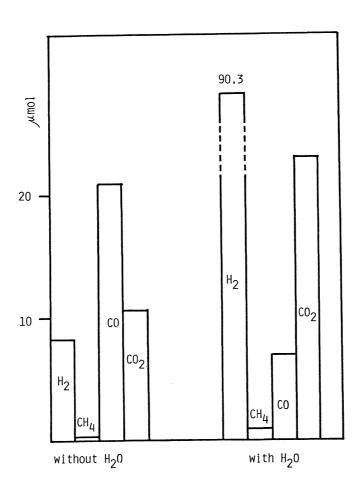


Fig 1. The amount of gases produced by the reaction of cellulose (13.6 mg) without and with $\rm H_2O$ vapor over $\rm Ru/SiO_2$ (0.015 g) at 300°C for 300 min.

It is of great interest to note that when KOH $(1.75 \times 10^{-3} \text{ mol})$ was added to the system, a marked increase in the reactivity and the changes in the reaction products were observed. It was revealed that the amount of CO was less and higher hydrocarbons, ethylene and propylene, were produced with high selectivity (Table 1). The decomposition temperature of cellulose became lower in the presence of KOH or NaOH, in the cellulose sample^{2,3)}, which suggests that the alkali metal ions play an important role in breaking the cellulose skelton, and increase the reactivity of cellulose with water. Since the amount of CO was less when KOH was added to the system, CH_4 formation over Ru catalyst was restrained than that in the case of neutral system.

The reaction mechanism can be considered as follows.

$$H_2O + CO \xrightarrow{\text{cat.}} H_2 + CO_2$$
 (2)

$$3H_2 + CO \xrightarrow{Ru} CH_4 + H_2O$$
 (3)

Cellulose itself decomposes to form CO, ${\rm CO_2}$ and ${\rm H_2O}$ at the first stage (1), followed by the water gas shift reaction over catalysts, which produces ${\rm H_2}$ (2). And the produced ${\rm H_2}$ and CO reacted to form ${\rm CH_4}$ in the case of Ru catalyzed reaction (3).

It is thus demonstrated here that the carbohydrates, which are annually reproducible in a short time cycle, can be easily converted into hydrocarbon and hydrogen by the reaction with water in the presence of Pt or Ru catalysts. H_2 , CO and CO_2 were mainly produced over Pt catalyst, while H_2 , CH_4 and CO_2 over Ru catalyst. The importance of methane formation may be emphasized in comparison with the photocatalytic reaction by $Pt/TiO_2/RuO_2$ recently reported, in which H_2 and CO_2 are the main products 4).

References

- 1) M. A. Vannice, J. Catalysis, <u>37</u>, 449 (1975).
- 2) T. Tachibana, J. Chem. Soc. Japan, 63, 924 (1942).
- 3) K. Tamaru, Bull. Chem. Soc. Japan, 24, 164 (1951).
- 4) T. Kawai and T. Sakata, Nature, 286, 474 (1980).

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